

September 1, 1969

9100B THERMODYNAMICS PROGRAM LISTING

73851 - HEAT TRANSFER THROUGH A MULTILAYERED CYLINDER

This program calculates the rate of heat flow through a multilayered cylinder. Both convective and conductive layers are considered.

9100B ONLY

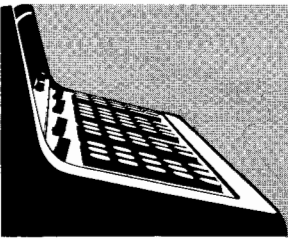
73852 - TRANSIENT CONDUCTION IN A SLAB

Given the initial temperature of a slab and a fluid, this program determines the temperature (as a function of time and distance) of the slab as it is immersed into the fluid.



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PART NO.
09100-73851

HEAT TRANSFER THROUGH A MULTILAYERED CYLINDER

This program determines the rate of heat flow per unit length through a multilayered cylinder. It has practical application wherever fluids of different temperatures are separated by a cylindrical surface since both convective and conductive layers are considered.

The basic equation is:

$$q = U_n A (\Delta T)$$

where

$$A = 2\pi \cdot r_o L,$$

and

$$U_n = \frac{1}{\left(\frac{r_o}{r_{c1} h_1} + \frac{r_o}{r_{c2} h_2} + \dots \right) + \left(\frac{r_o \ln \left(\frac{r_{o1}}{r_{i1}} \right)}{k_1} + \frac{r_o \ln \left(\frac{r_{o2}}{r_{i2}} \right)}{k_2} + \dots \right)}$$

Nomenclature

- U_n - Outside over-all heat transfer coefficient
- r_o - Outside radius of the cylinder
- k_n - Thermal conductivity of a conductive layer
- r_{on} - Outside radius of a conductive layer
- r_{in} - Inside radius of a conductive layer
- h_n - Film coefficient of a convective layer
- r_{cn} - Radius to a convective surface
- ΔT - Temperature difference (inside - outside)
- q - Heat transfer rate

Reference: Heat Transfer, Alan J. Chapman, Macmillan Company, New York, 1967.

USER INSTRUCTIONS

EXAMPLES

PRESS: END

ENTER PROGRAM: (Starting Address is 0-0)

PRESS: END

PRESS: CONTINUE

DISPLAY

0 _____ Z
0 _____ Y
0 _____ X

ENTER DATA: $r_o \rightarrow Z$, $T_o \rightarrow Y$, $T_i \rightarrow X$

PRESS: CONTINUE

DISPLAY

0 _____ Z
0 _____ Y
n _____ X

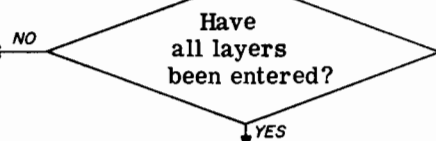
n is the
layer to
be entered

ENTER DATA: For conductive layer
 $k \rightarrow Z$, $r_{on} \rightarrow Y$, $r_{in} \rightarrow X$

For convective layer
 $0 \rightarrow Z$, $h \rightarrow Y$, $r_{cn} \rightarrow X$

NOTE: A convective layer is considered very thin and only the radius to the convection surface is entered.

PRESS: CONTINUE



PRESS: SET FLAG

PRESS: CONTINUE

DISPLAY

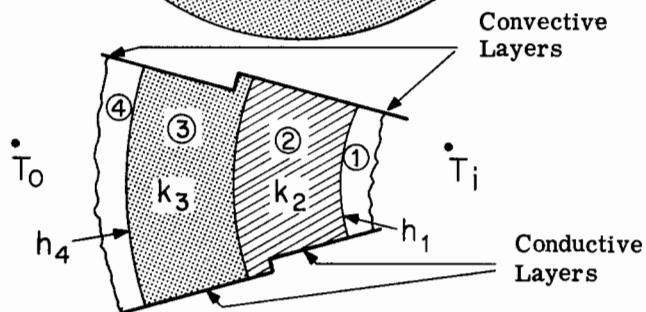
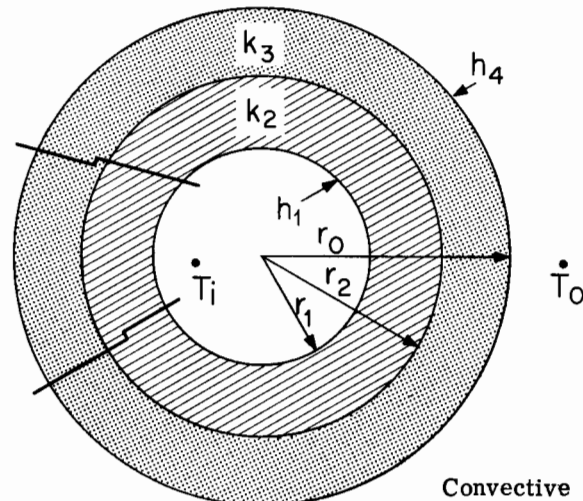
0 _____ Z
q/L _____ Y
0 _____ X

To run another problem

A.

$r_o = .833$ ft. $T_o = 100^\circ$ F
 $r_2 = .667$ ft. $T_i = 500^\circ$ F
 $r_1 = .500$ ft.
 $h_1 = 300$ Btu/hr. ft.² °F
 $k_2 = 40$ Btu/hr. ft. °F
 $k_3 = .10$ Btu/hr. ft. °F
 $h_4 = 6$ Btu/hr. ft.² °F

4 LAYER PROBLEM



DATA ENTRY: $.833 \rightarrow Z$, $100 \rightarrow Y$, $500 \rightarrow X$

Layer	X	Y	Z
1	.500	300	0
2	.500	.667	40
3	.667	.833	.10
4	.833	6	0

Results: $q/L = 1031.558$ Btu/hr. ft.

B. Same as above except $k_3 = .01$ Btu/hr. ft. °F
(Better insulation).

Results: $q/L = 112.008$ Btu/hr. ft.

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Step	Key	Code	Display			Step	Key	Code	Display			Step	Key	Code	Display		
			x	y	z				x	y	z				x	y	z
0	CLEAR	20	ENTER			3	ROLL ↑	22				0					
(+) 1	STOP	41	T _i	T ₀	r ₀	(+) 1	÷	35				1					
2	x↔y	30				2	d	17				2					
3	—	34				3	÷	35				3					
4	y→()	40				4	0	00				4					
5	b	14				5	ACC +	60				5					
6	↓	25				6	↑	27				6					
7	y→()	40				7	↑	27				7					
8	a	13				8	GO TO ()	44				8					
9	CLEAR	20				9	0	00				9					
a	1	01				a	a	13				a					
b	ACC +	60	ENTER			b	1	01				b					
c	f	15	r _{cn}	h	0	c	↑	27				c					
d	STOP	41	r _{in}	r _{on}	k	d	E	12				d					
1	IF FLAG	43				4	÷	35				0					
(+) 1	3	03				(+) 1	2	02				1					
2	b	14				2	x	36				2					
3	x→()	23				3	π	56				3					
4	d	17				4	x	36				4					
5	0	00				5	a	13				5					
6	ROLL ↑	22				6	x	36				6					
7	IF x=y	50				7	b	14				7					
8	2	02				8	x	36				8					
9	d	17				9	CLEAR x	37				9					
a	ROLL ↓	31				a	CONT	47	DISPLAY			a					
b	d	17				b	END	46	0	q/L	0	b					
c	÷	35				c						c					
d	a	13				d						d					
2	x↔y	30				0						Storage					
(+) 1	ln x	65				1						f					
2	x	36				2						e					
3	↓	25				3						d					
4	x↔y	30				4						c					
5	÷	35				5						b					
6	0	00				6						a					
7	ACC +	60				7						9					
8	↑	27				8						8					
9	↑	27				9						7					
a	GO TO ()	44				a						6					
b	0	00				b						5					
c	a	13				c						4					
d	a	13				d						3					
												2					
												1					
												0					

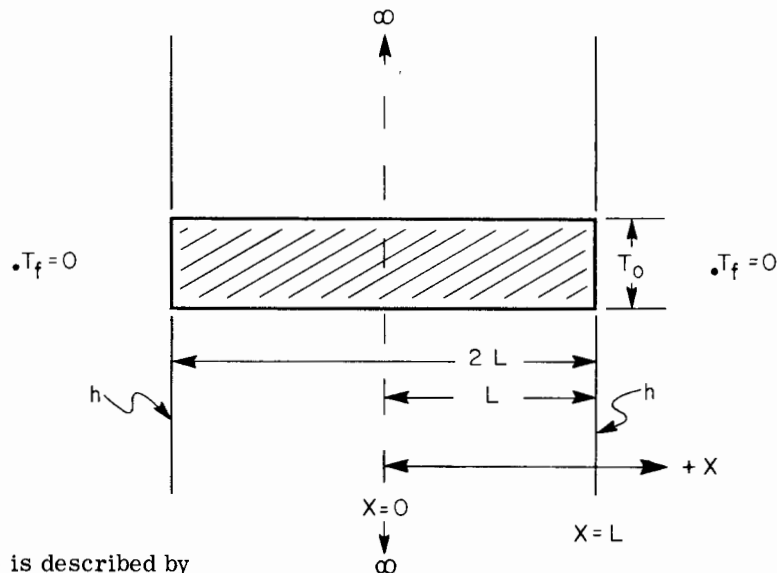
Step	Key	Code	Display			Step	Key	Code	Display			Step	Key	Code	Display		
			x	y	z				x	y	z				x	y	z
0						0						0					
1						1						1					
2						2						2					
3						3						3					
4						4						4					
5						5						5					
6						6						6					
7						7						7					
8						8						8					
9						9						9					
a						a						a					
b						b						b					
c						c						c					
d						d						d					
0						0						0					
1						1						1					
2						2						2					
3						3						3					
4						4						4					
5						5						5					
6						6						6					
7						7						7					
8						8						8					
9						9						9					
a						a						a					
b						b						b					
c						c						c					
d						d						d					
0						0						Storage					
1						1						f					
2						2						e					
3						3						d					
4						4						c					
5						5						b					
6						6						a					
7						7						9					
8						8						8					
9						9						7					
a						a						6					
b						b						5					
c						c						4					
d						d						3					
												2					
												1					
												0					

9100B ONLY
PART NO.
09100-73852

TRANSIENT CONDUCTION IN A SLAB

This program calculates, as a function of time and position, the temperature of a plane in a slab which has been heated to an initial temperature and then placed in a fluid of a different temperature. This is equivalent to plunging a heated bar into a quenching medium. The program assumes the slab is infinite, therefore, the problem involves one dimensional transient conduction.

The temperature of the fluid is taken to be zero and used as a reference. For example, if the temperature of the fluid is actually 40°F and the slab is initially at 100°F, the user would input 60°F (100 - 40) as the initial temperature of the slab. The actual temperature of a plane in the slab at a later time is then the calculated value plus 40°F (see example B).



The temperature is described by

$$T = 2T_0 \sum_{n=1}^{\infty} e^{-\lambda_n^2 \alpha \tau} \frac{\sin(\lambda_n L)}{\lambda_n L + \sin(\lambda_n L) \cos(\lambda_n L)} \cdot \cos(\lambda_n X)$$

where λ_n is the n th root of

$$(\lambda_n L) \tan(\lambda_n L) - N_{Bi} = 0$$

and N_{Bi} is the Biot modulus ($N_{Bi} = h L/k$).

Reference: Heat Transfer, Alan J. Chapman
Macmillan Company, New York, 1967.

Nomenclature:

T_o	-	Initial temperature of the slab
α	-	Thermal diffusivity of the slab
k	-	Thermal conductivity of the slab
h	-	Film coefficient
L	-	One-half the width of the slab
τ	-	Independent time variable
X	-	Independent space variable
T	-	Dependent temperature variable
T_f	-	Temperature of the fluid

- NOTES: 1. The program performs the summation until adding the next term changes it less than 10^{-5} . To change this tolerance go to location (-5)(d) and enter the desired exponent.
2. The calculation of the roots ($\lambda_n L$) may be seen by placing a PAUSE at location (1) (c). The root ($\lambda_n L$) is displayed in the X register as the solution converges. Place a STOP at location (4)(1) for a display of the calculated root in the X register.
3. The execution time is about two minutes.

USER INSTRUCTIONS

EXAMPLES

SET: ☐ RADIANS

PRESS: END

ENTER PROGRAM: Side A followed by Side B

PRESS: CONTINUE

DISPLAY

0 ——— Z
0 ——— Y
1 ——— X

ENTER DATA: $N_{Bi} \rightarrow Z$, $T_o \rightarrow Y$, $L \rightarrow X$

PRESS: CONTINUE

DISPLAY

0 ——— Z
0 ——— Y
2 ——— X

ENTER DATA: $\alpha \rightarrow Z$, $\tau \rightarrow Y$, $X \rightarrow X$

PRESS: CONTINUE

DISPLAY

T ——— Z
n ——— Y
X ——— X

n is the number
of terms used
in the summation

To re-run problem with different X , τ , or α :

PRESS: CONTINUE

To run new problem:

PRESS: END

NOTE: Any consistent set of units may be used.

A.

$N_{Bi} = 20$
 $T_o = 120^\circ\text{F}$ ($T_f = 0^\circ\text{F}$)
 $L = .4 \text{ ft.}$
 $\alpha = .02 \text{ ft.}^2/\text{hr.}$
 $\tau = 1 \text{ hr.}$
 $X = .1 \text{ ft.}$

Results

$T = 105.49^\circ\text{F}$
 $n = 4$
 $X = .1 \text{ ft.}$



B.

$N_{Bi} = 20$
Temperature of the slab initially is 180°F
Temperature of the fluid is 30°F
 $T_o = 180^\circ - 30^\circ = 150^\circ\text{F}$
 $L = .4 \text{ ft.}$
 $\alpha = .02 \text{ ft.}^2/\text{hr.}$
 $\tau = 1 \text{ hr.}$
 $X = .1 \text{ ft.}$

Results

$T = 131.87^\circ\text{F}$
 $n = 4$
 $X = .1 \text{ ft.}$
Actual temperature is $T + 30^\circ\text{F} = 161.87^\circ\text{F}$

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Step	Key	Code	Display			Step	Key	Code	Display			Step	Key	Code	Display		
			x	y	z				x	y	z				x	y	z
0	GOTO ()	44				3	1	01				8	CLEAR	20			
(+)	1	8				(+)	1	$y \rightarrow ()$	24			(+)	1	01	ENTER		
2	0	00				2	7	07				2	STOP	41	L	T ₀	NBi
3	.	21				3	X	36				3	$x \rightarrow ()$	23			
4	1	01				4	$y \rightarrow ()$	40				4	—	34			
5	$x \rightarrow ()$	23				5	7	07				5	f	15			
6	7	07				6	d	17				6	$y \rightarrow ()$	40			
7	C	16				7	+	33				7	—	34			
8	GOTO ()	44				8	IF $x=y$	50				8	C	16			
9	0	00				9	0	00				9	ROLL $\uparrow$	22			
a	C	16				a	b	14				a	$x \rightarrow ()$	23			
b	SET FLAG	54				b	$\downarrow$	25				b	b	14			
c	$x \rightarrow ()$	23				c	GOTO ()	44				c	CLEAR	20			
d	d	17				d	0	00				d	$x \rightarrow ()$	23			
1	$\uparrow$	27				4	C	16				9	—	34			
(+)	1	tan x	71			(+)	1	CONT	47			(+)	a	13			
2	X	36				2	$\uparrow$	27				2	$x \rightarrow ()$	23			
3	b	14				3	$x \leftarrow ()$	67				3	—	34			
4	—	34				4	C	16				4	b	14			
5	$\downarrow$	25				5	$\uparrow$	27				5	$x \rightarrow ()$	23			
6	$\uparrow$	27				6	π	56				6	C	16			
7	$y \rightarrow ()$	24				7	+	33				7	GOTO ()	44			
8	6	06				8	$y \rightarrow ()$	40				8	—	34			
9	X	36				9	C	16				9	0	00			
a	$\uparrow$	27				a	$\downarrow$	25				a	0	00			
b	d	17				b	CHG SIGN	32				b	CONT	47			
c	CONT	47				c	$x \rightarrow ()$	23				c	CONT	47			
d	IF FLAG	43				d	6	06				d	CONT	47			
2	4	04				5	$\downarrow$	25				Storage					
(+)	1	01				(+)	1	RETURN	77			+ -					
2	ROLL $\downarrow$	31				2						F				L	
3	CLEAR x	37				3						E				a	T
4	IF $x < y$	52				4						d				X	
5	3	03				5						c	n π			T ₀	
6	0	00				6						b	NBi			n	
7	IF $x=y$	50				7						a				Σ	
8	ROLL $\uparrow$	22				8						9					
9	GOTO ()	44				9						8					
a	0	00				a						7					
b	b	14				b						6					
c	CHG SIGN	32				c						5					
d	.	21				d						4					
												3					
												2					
												1					
												0					

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Step	Key	Code	Display			Step	Key	Code	Display			Step	Key	Code	Display		
			x	y	z				x	y	z				x	y	z
00	2	02				30	—	34				60	CHG SIGN	32			
(-) 1	CHG SIGN	32				(-) 1	9	11				(-) 1	IF $x > y$	53			
2	$x \rightarrow ()$	23				2	$x \leftarrow ()$	67				2	6	06			
3	6	06				3	—	34				3	7	07			
4	CHG SIGN	32	ENTER			4	f	15				4	GO TO ()	44			
5	STOP	41	X	T	a	5	$\div$	35				5	1	01			
6	$x \rightarrow ()$	23				6	$\downarrow$	25				6	0	00			
7	—	34				7	$\uparrow$	27				7	$x \leftarrow ()$	67			
8	d	17				8	x	36				8	—	34			
9	ROLL $\downarrow$	31				9	$x \leftrightarrow y$	30				9	a	13			
a	x	36				a	$\uparrow$	27				a	$\uparrow$	27			
b	$y \rightarrow ()$	40				b	$x \leftarrow ()$	67				b	2	02			
c	—	34				c	—	34				c	x	36			
d	e	12				d	e	12				d	$x \leftarrow ()$	67			
10	$x \leftarrow ()$	67				40	x	36				70	—	34			
(-) 1	—	34				(-) 1	$\downarrow$	25				(-) 1	c	16			
2	b	14				2	CHG SIGN	32				2	x	36			
3	$\uparrow$	27				3	e^x	74				3	$x \leftarrow ()$	67			
4	1	01				4	$y \leftrightarrow ()$	24				4	—	34			
5	+	33				5	—	34				5	b	14			
6	$y \rightarrow ()$	40				6	9	11				6	$\uparrow$	27			
7	—	34				7	x	36				7	$x \leftarrow ()$	67			
8	b	14				8	$x \leftarrow ()$	67				8	—	34			
9	GO TO ()	44				9	—	34				9	d	17			
a	Δ SUB ∇	77				a	d	17				a	CONT	47	DISPLAY		
b	+	33				b	ROLL $\uparrow$	22				b	STOP	41	X	n	T
c	0	00				c	x	36				c	GO TO ()	44			
d	3	03				d	CLEAR x	37				d	+	33			
20	$x \rightarrow ()$	23				50	$\downarrow$	25				Storage					
(-) 1	—	34				(-) 1	cos x	73				f					
2	9	11				2	x	36				e					
3	CLEAR x	37				3	$x \leftarrow ()$	67				d					
4	$\downarrow$	25				4	—	34				c					
5	cos x	73				5	a	13				b					
6	$x \leftrightarrow y$	30				6	+	33				a					
7	sin x	70				7	$y \rightarrow ()$	40				9					
8	x	36				8	—	34				8					
9	ROLL $\downarrow$	31				9	a	13				7					
a	+	33				a	—	34				6					
b	$\downarrow$	25				b	y	55				5					
c	$\div$	35				c	ENTER EXP	26				4					
d	$y \leftrightarrow ()$	24				d	5	05				3					
												2					
												1					
												0					

 HEWLETT · PACKARD

Step	Key	Code	Display			Step	Key	Code	Display			Step	Key	Code	Display		
			x	y	z				x	y	z				x	y	z
8	0	8	10			0						0					
(-)	1	L	16			1						1					
	2	END	46			2						2					
	3					3						3					
	4					4						4					
	5					5						5					
	6					6						6					
	7					7						7					
	8					8						8					
	9					9						9					
	a					a						a					
	b					b						b					
	c					c						c					
	d					d						d					
	0					0						0					
	1					1						1					
	2					2						2					
	3					3						3					
	4					4						4					
	5					5						5					
	6					6						6					
	7					7						7					
	8					8						8					
	9					9						9					
	a					a						a					
	b					b						b					
	c					c						c					
	d					d						d					
	0					0						Storage					
	1					1						f					
	2					2						e					
	3					3						d					
	4					4						c					
	5					5						b					
	6					6						a					
	7					7						9					
	8					8						8					
	9					9						7					
	a					a						6					
	b					b						5					
	c					c						4					
	d					d						3					
												2					
												1					
												0					

Step	Key	Code	Display			Step	Key	Code	Display			Step	Key	Code	Display		
			x	y	z				x	y	z				x	y	z
0						0						0					
1						1						1					
2						2						2					
3						3						3					
4						4						4					
5						5						5					
6						6						6					
7						7						7					
8						8						8					
9						9						9					
a						a						a					
b						b						b					
c						c						c					
d						d						d					
0						0						0					
1						1						1					
2						2						2					
3						3						3					
4						4						4					
5						5						5					
6						6						6					
7						7						7					
8						8						8					
9						9						9					
a						a						a					
b						b						b					
c						c						c					
d						d						d					
0						0						Storage					
1						1						F					
2						2						E					
3						3						D					
4						4						C					
5						5						B					
6						6						A					
7						7						9					
8						8						8					
9						9						7					
a						a						6					
b						b						5					
c						c						4					
d						d						3					
												2					
												1					
												0					